

# Content of Lecture

1. Phenomenology of Combustion
2. Thermodynamic Fundamentals
3. Chemical Reaction Kinetics
4. Ignition and Ignition Limits
5. Laminar Flame Theory
- 6. Turbulent Combustion**
7. Pollutants of Combustion
8. Combustion of Liquid and Solid Fuels
9. Numerical Simulation
10. Measurement Techniques of Combustion Processes
11. Applied Aspects of Turbulent Combustion
12. Technical Burner Systems
13. Internal Combustion Engines

## 6. Fundamentals of turbulent combustion

### 6.0 Motivation for turbulent combustion

### 6.1 Turbulence quantities

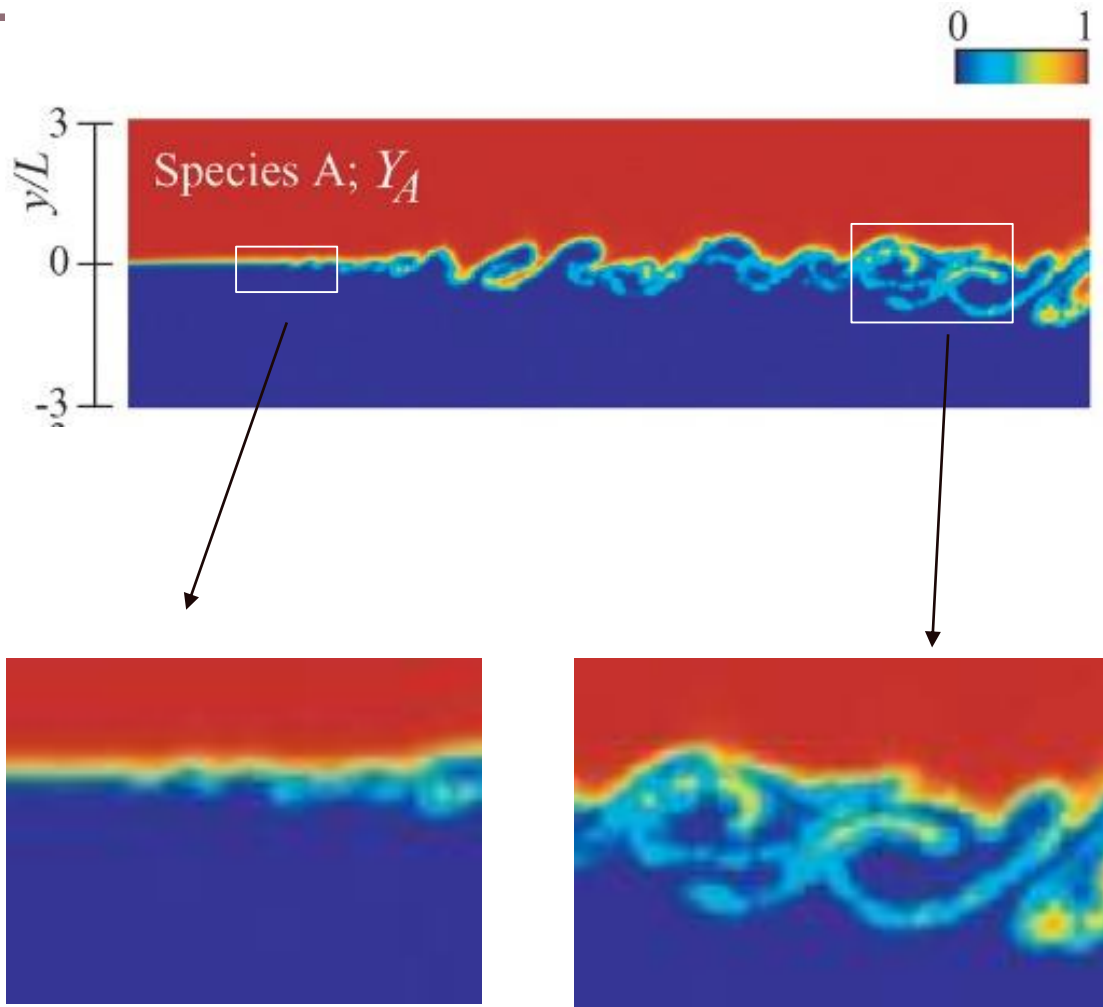
### 6.2 Turbulent premixed flames

- The Borghi diagram
- Structure of turbulent flames
- Turbulent flame speed
- Approaches for calculation

### 6.3 Turbulent diffusion flames

- Examples
- Flame length
- Concept of mixture fraction

# Motivation for turbulent combustion



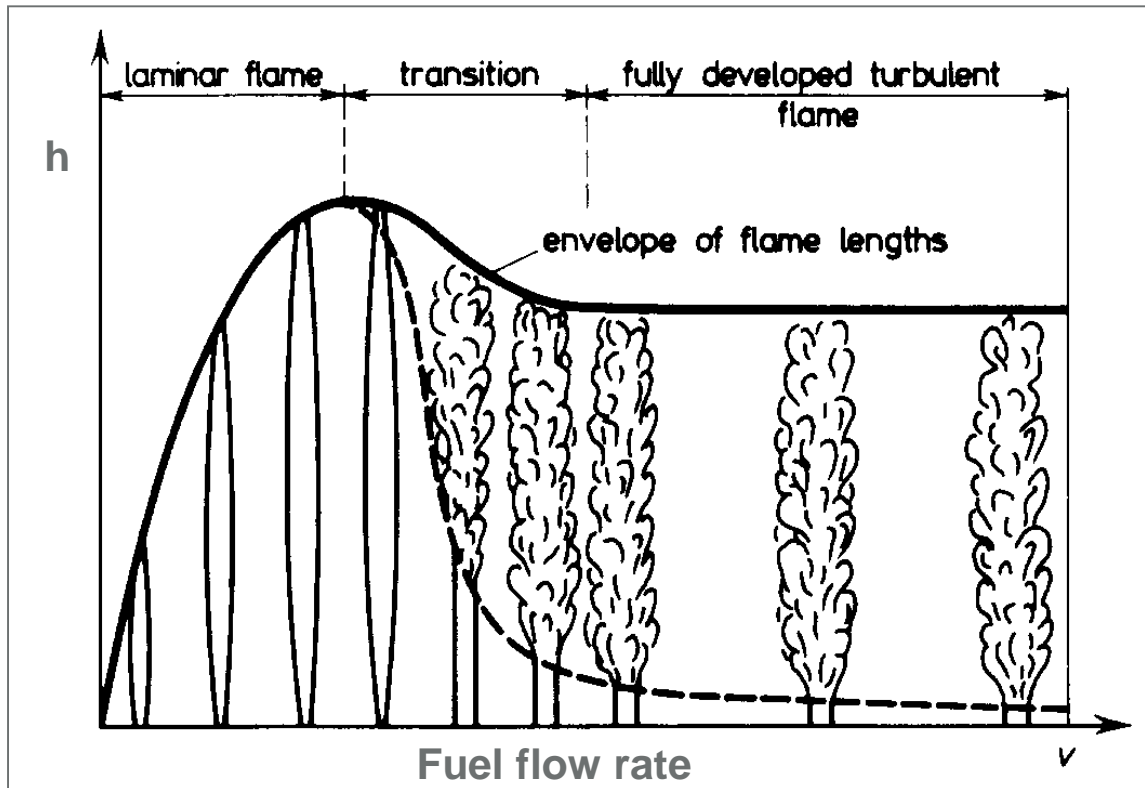
- Two flows of two species at different velocities behind splitter plate
- Shear at interface lead to formation of eddies, which grow.
- Fluid B convected upward, and Fluid A convected downward
- Interfacial area over which diffusion occurs is increased  
->enhanced mixing

# Motivation for turbulent combustion

## 6.0 Motivation for turbulent combustion

### Why turbulent combustion ?

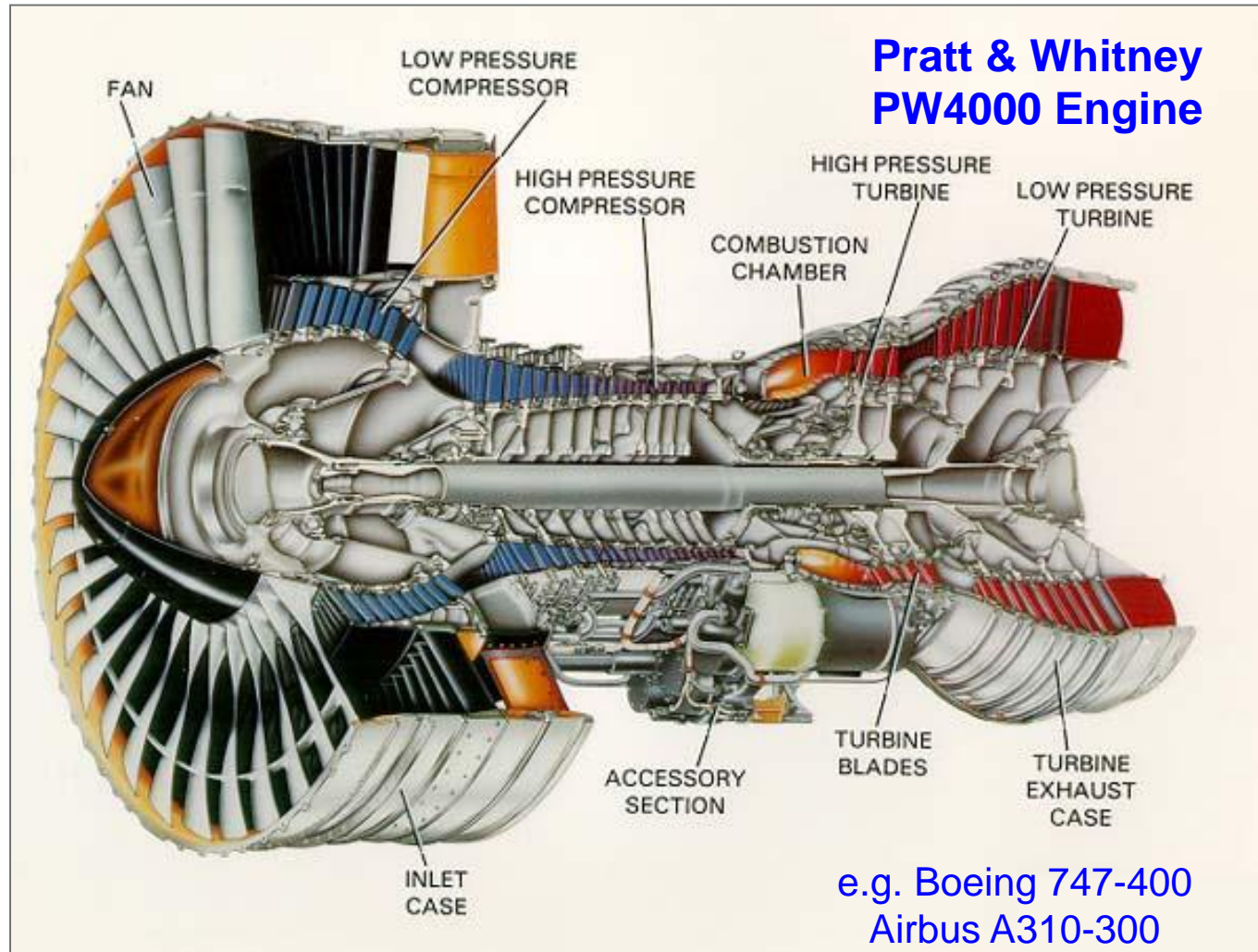
- Mixing is enhanced  $\longrightarrow$  Heat release per volume (power density) increases  $\longrightarrow$  smaller burning chambers possible (engine, airplane engine)



fol. Hottel u. Hawthorne,  
3. Comb. Symp. (1949)

# Motivation for turbulent combustion

## Why turbulent combustion ?



# Turbulence quantities

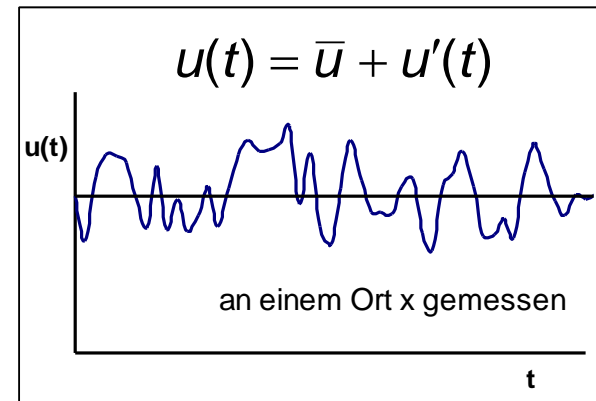
## 6.2 Turbulence Quantities

### Turbulent Flow:

- time dependent fluctuating velocities
- three dimensional
- eddy structures (e.g. *Karman's eddy street*)

### 2 possible approaches:

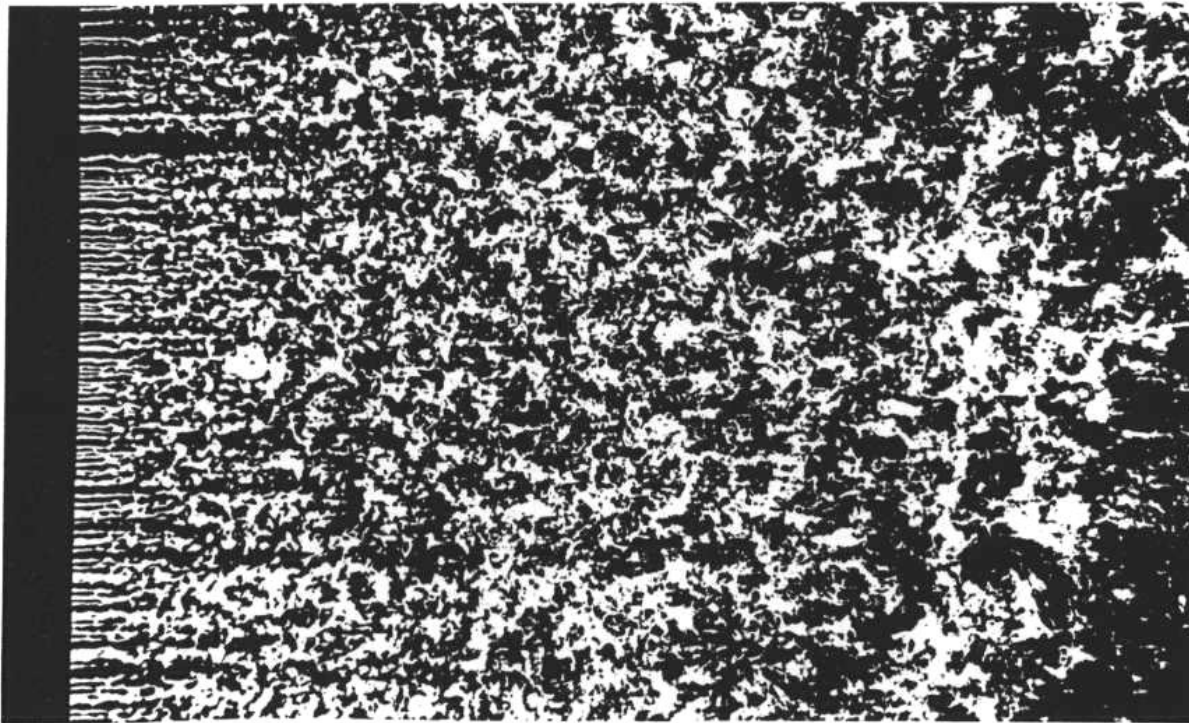
- **statistical**
  - -> Mean value
  - -> Standard deviation etc.
- **structural**
  - eddy description, LES, DNS



## Homogeneous Turbulence

Idealization: Homogeneous isotropic turbulence (assumed in the following)

- In reality only as approximation:
- 1: Stirred chamber with strong mixing without swirl
- 2: "Grid turbulence " = "Wind channel turbulence"



153. Homogeneous turbulence behind a grid. Behind a finer grid than above, the merging unstable wakes quickly form a homogeneous field. As it decays down-

stream, it provides a useful approximation to the idealization of isotropic turbulence. *Photograph by Thomas Corke and Hassan Nagib*

## Homogeneous Turbulence

Common statistical approach: Reynolds decomposition

*Mean value*

$$u(t) = \bar{u} + u'(t) \quad (6.1)$$

$$\overline{u'(t)} = 0 \quad (6.3)$$

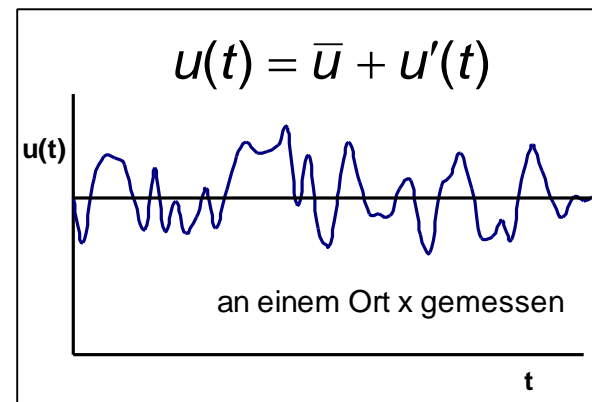
$$u' \equiv u'_{rms} = \sqrt{\overline{(u'(t))^2}} \quad (6.2)$$

*"Turbulence intensity" (Fluctuation velocity =  
Root-Mean-Square Velocity)*

*"Turbulence degree" (v. Kármán Number)*

$$Tu \equiv \frac{u'}{\bar{u}} \quad (6.4)$$

(typ.  $Tu < 10\%$  for grid turbulence )

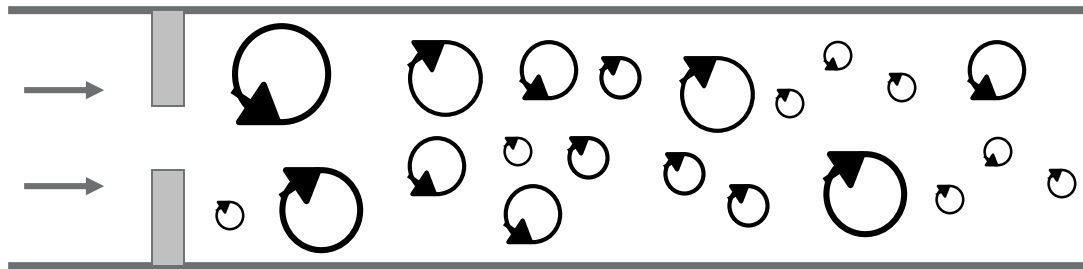


# Turbulence quantities

## Concept of Eddy cascade

Eddies of different size

"Concept of eddy cascade" (eddy spectrum)



*Hindrance -> Large eddies -> smaller eddies -> very small eddies*

*(Energy transport = Dissipation rate  $\varepsilon$ )*

*-> Molecular dissipation  
(to heat)*

**"Integral length scale"  $L_x$**   
(*"Macro length scale"*)

**"Kolmogorov-scale"  $\eta$  (or  $l_k$ )**  
(*"Micro length scale"*)

# Turbulence quantities

## Transition laminar - turbulent

**Reynolds number**  $Re = \frac{\bar{u} \cdot D}{\nu}$  (6.5)

Note: depends on geometry !

$D$  = geometrical size

$\nu$  = kin. viscosity

$Re_{kr} \approx 2200$   
100 - 1000

Flow in tube  
Axial free jet flow

### "Turbulent Reynolds number"

$Re_t = \frac{u' \cdot L_x}{\nu}$  (6.6)

Independent from geometry !  
characteristic local quantity

turbulent:  $Re_t > 1$

Note:  $Re_t$  is about 100 - 1000 times smaller than  $Re$

# Turbulence quantities

## Turbulence characterization:

(Assumption: fully developed turbulence, homogeneous, isotropic)



Turbulent fluctuation velocity  $u' = u_{rms}$  (measured)

Integral length scale (Macro length)  $L_x$  (measured)

Turbulent Reynolds number  $Re_t = u' L_x / \nu$  (6.7)

Kolmogorov length (Micro length)  $\eta = L_x / Re_t^{3/4}$  (6.8)

Increase of turbulent Reynolds number broadens turbulence spectrum

Note aside: in some articles the Taylor length is used:

Taylor length  $l_\lambda = 6,3 L_x / Re_t^{1/2}$  (6.9)

Local mean turbulent strain rate  $a = u' / l_\lambda$  (6.10)

(Scherrate)

# Turbulent premixed flames

## 6.2 Turbulent premixed Flames

### Turbulent premixed flames

- Fuel and air are premixed
- Danger of flash back
- Lean premixed flames can have low pollutant emissions:
  - No soot
  - Very low  $\text{NO}_x$  formation (stationary gas turbines, 'Blue burner')
- **Turbulence increases the density of reaction ( $P_{\text{thermal}} / V_{\text{flame}}$ ). How ?**

6.2.1 Structure of turbulent premixed flames

6.2.2 The Borghi diagram

6.2.3 Turbulent flame speed

6.2.4 Flamelet model for calculation of turbulent premixed flames

# Turbulent premixed flames

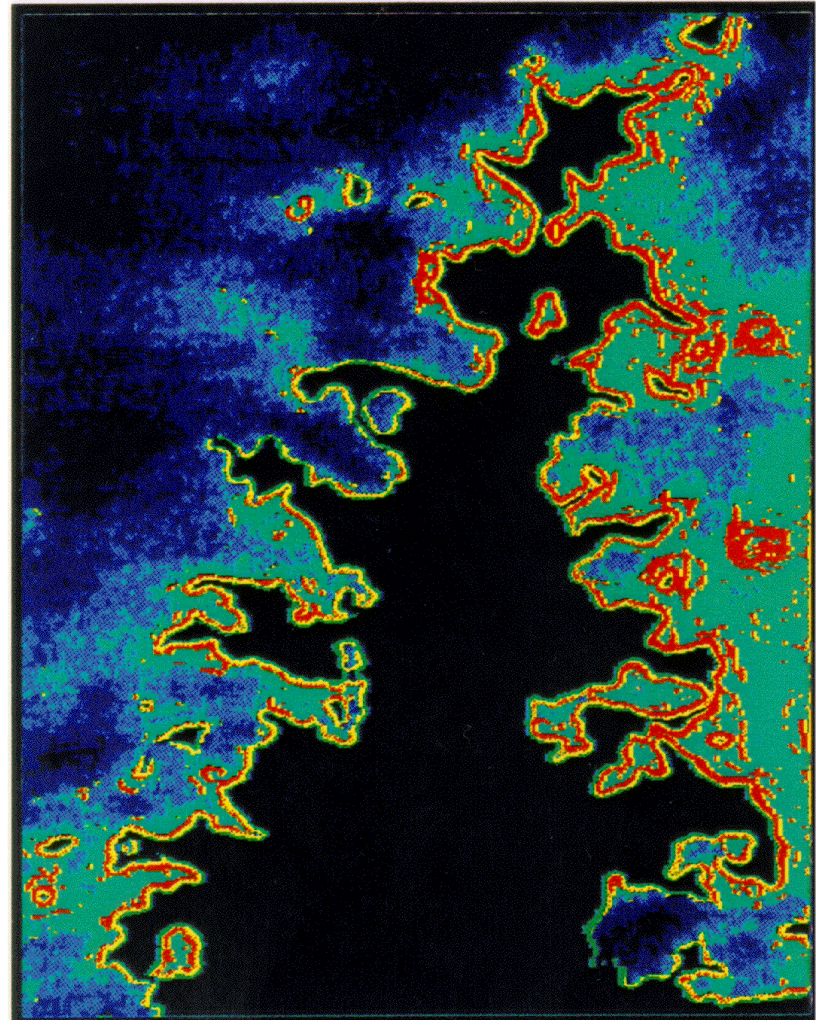
## Turbulent premixed flames



Bunsen  
flame  
(Heidelberg)

$D=80$  mm  
100 kW

Photograph:  
Laser-  
diagnostics  
(15x10 cm)



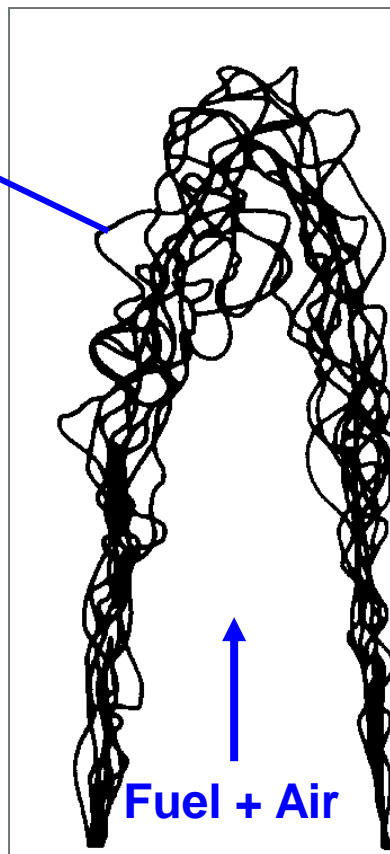
# Turbulent premixed flames

## Turbulent premixed flames

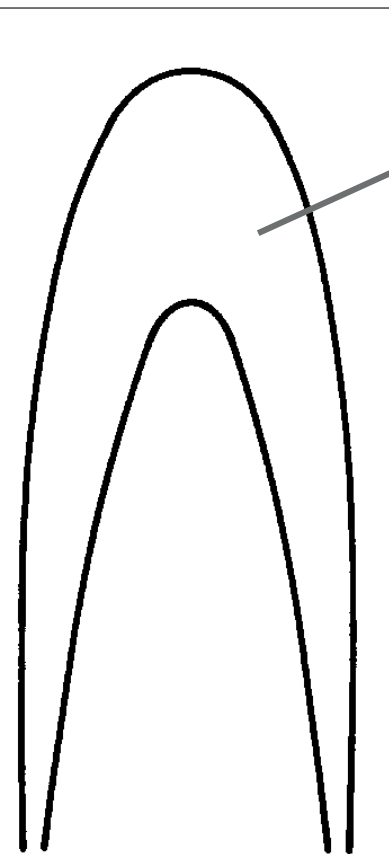
Several instantaneous images

Average image

**Flame front**  
(Flammenfront)



**Flame brush**  
(Flammenzone)



# Turbulent premixed flames

## Turbulence - Flame Interaction

→ **Turbulent flow field has strong influence on premixed flames**

- Details of turbulence-flame interaction only barely known for long time.
- Theoretical analysis:

→ **Regime diagram following Borghi and Peters**

- Experimental verification was difficult for long time
  - Flame front fluctuates fast
  - Spatial flame structure  $< 1\text{mm}$

# Turbulent premixed flames

## Borghi diagram (Borghi 1985, Peters 1986)

Two Turbulence  
quantities:  $u'$ ,  $L_x$

Scaled with two laminar  
flame quantities  $s_L$ ,  $\delta_L$

Log. Scales

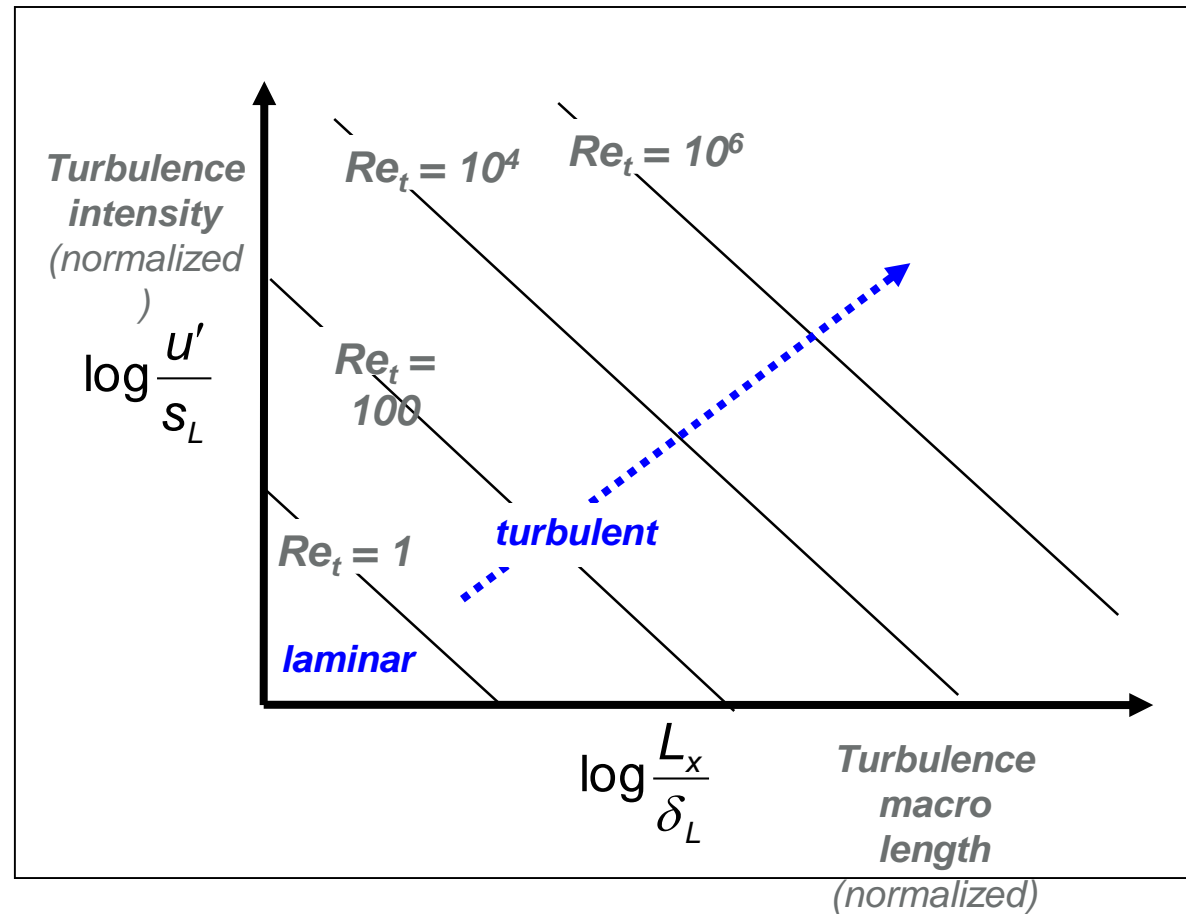
$$Re_t = u' L_x / \nu$$

indicates transition:  
laminar - turbulent  
and intensity of turbulence

Assumption:  $Le = a/D = 1$

and  $Sc = \nu/D = 1$

hence:  $\nu \approx a = s_L \cdot \delta_L^{Zeld}$



# Turbulent premixed flames

## Time Scales

### Turbulent Regime:

#### Two extreme Cases:

mixing time  $\ll$  reaction time

**"Stirred reactor"**

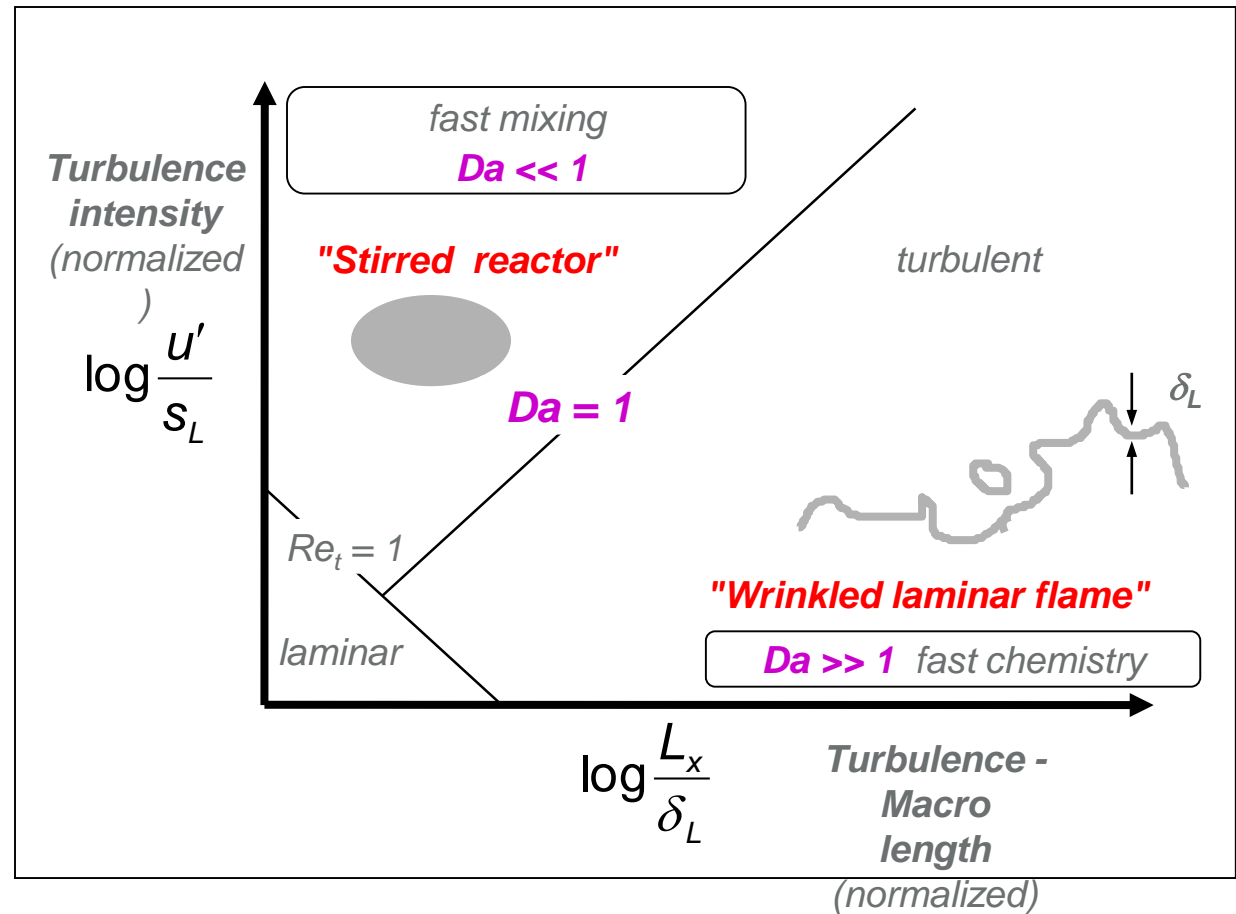
$Da \ll 1$

reaction time  $\ll$  mixing time

**"Wrinkled laminar flame"**

(however in a turbulent flow)

$Da \gg 1$



**Damköhler  
number**

$$Da = \frac{\tau_{turb}}{\tau_{reak}} = \frac{L_x / u'}{\delta_L / s_L} \quad (6.11)$$

(Turn over time of large eddy)  
(Transit time through lam. flame)

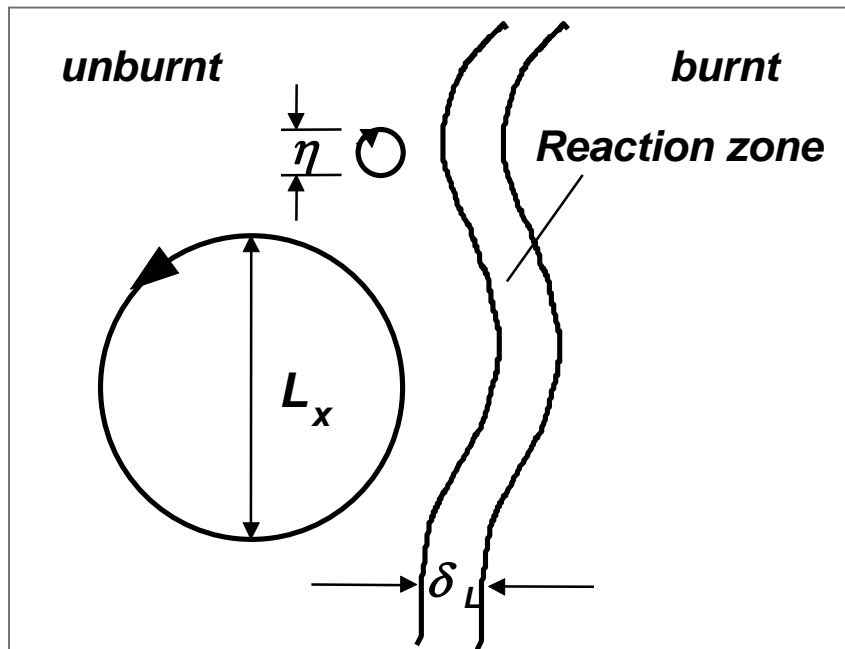
# Turbulent premixed flames

## Length Scales

### Model:

**Large Eddies** ( $l \gg \delta_L$ )  $\rightarrow$  wrinkle flame front

**Small Eddies** ( $l \ll \delta_L$ )  $\rightarrow$  enter the flame front, increase diffusive transport within the flame front  $\rightarrow$  they thicken the flame front



### Comparison of length scales:

#### Karlovitz number:

$$Ka = (\delta_L / \eta)^2 \quad (6.12)$$

with smallest "Kolmogorov-Eddies"

$$\eta = L_x / Re_t^{3/4}$$

# Turbulent premixed flames

## Distributed reaction zone

Model for the regime of distributed reaction zones

(*foll. Turns*)

Above which limit the smallest eddies enter the reaction zone ?

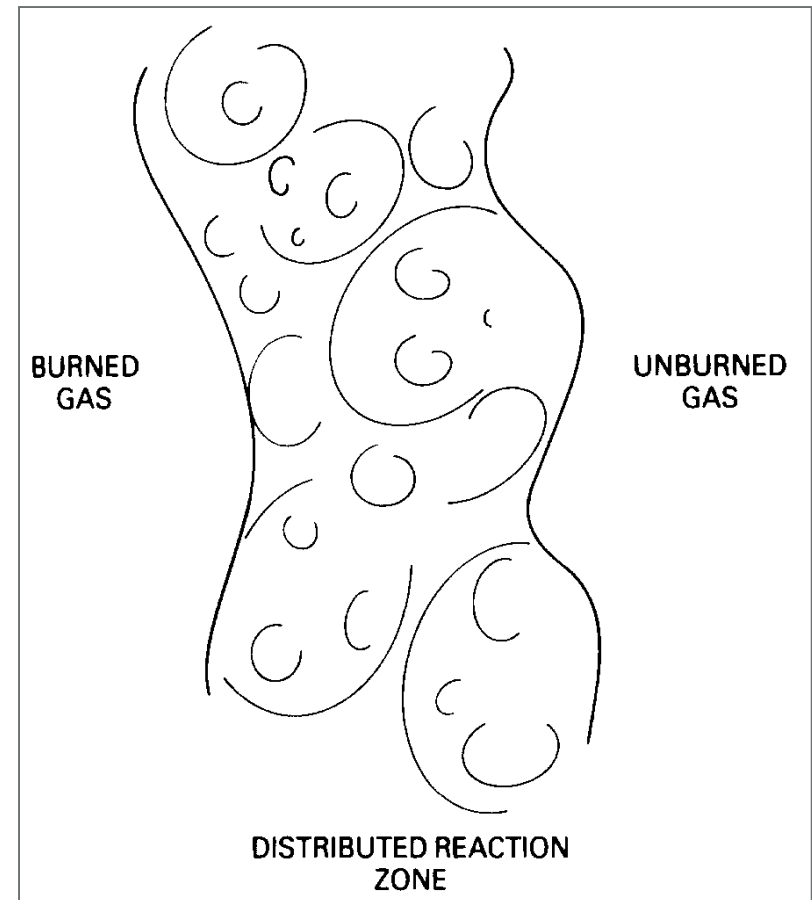
Supposition

("Klimov-Williams Criterion"):

Thickening, if  $\eta < \delta_L$

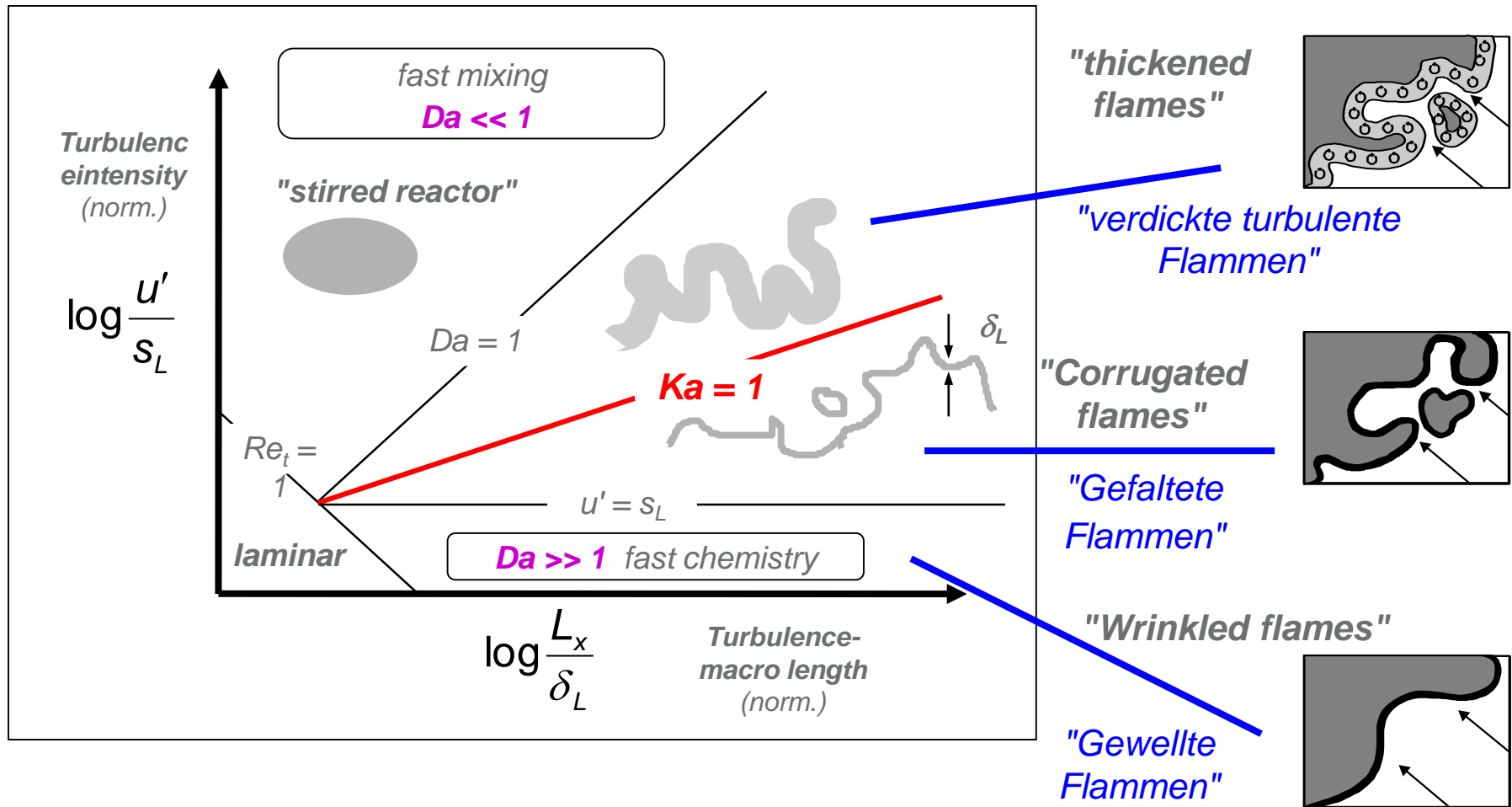
*i.e.*  $Ka > 1$

(6.13)



# Turbulent premixed flames

## Borghi diagram

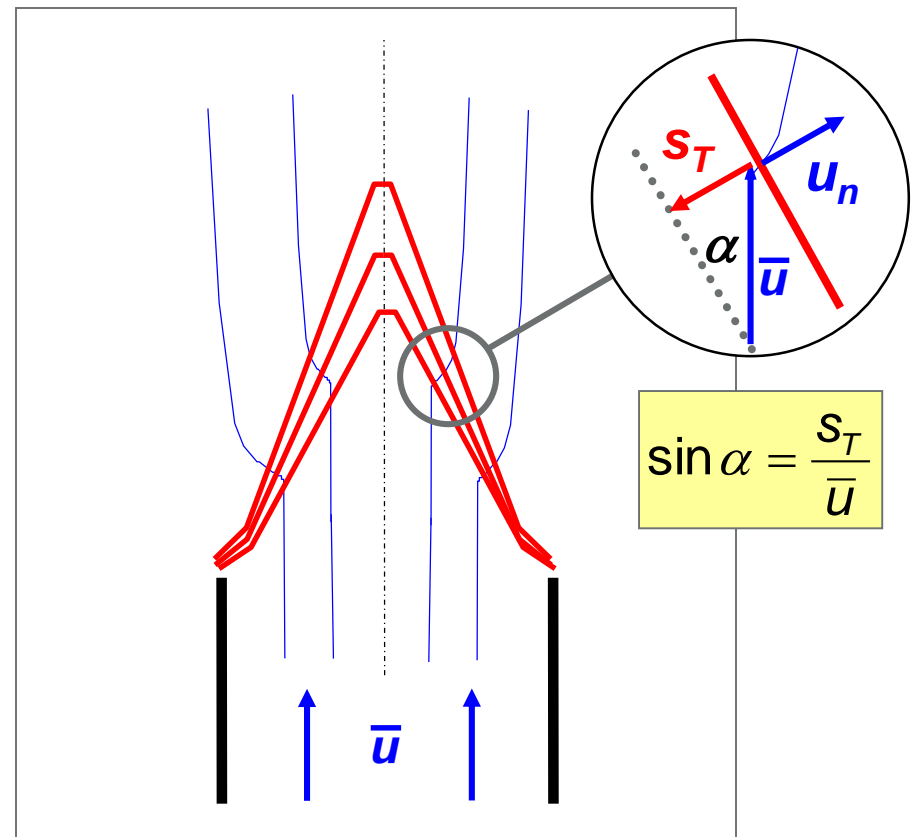


# Turbulent premixed flames

## Turbulent flame speed $s_T$

**Definition:** 'turbulent flame speed'  $s_T$

**Idea: Kinematic Balance** between turbulent flame speed  $s_T$  and the normal velocity component  $u_n$  for stationary flames.



# Turbulent premixed flames

## Turbulent flame speed $s_T$

### Height of flame

as approximation

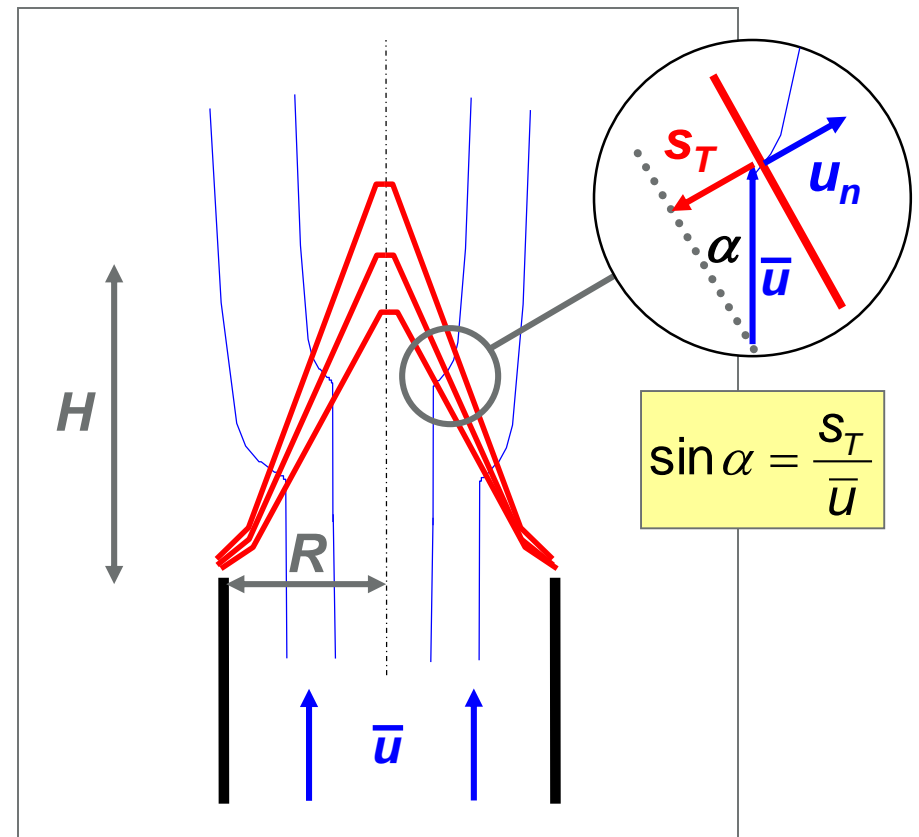
$$\sin \alpha = \frac{s_T}{\bar{u}} \quad (6.14)$$

with unburnt gas velocity  $\bar{u}$  and angle  $\alpha$  between  $\mathbf{u}$  and flame front.

For Bunsen flame (assumed  $\mathbf{u} = \text{const.}$ ) follows with

$$\tan \alpha = \frac{R}{H} \quad (6.15)$$

as (rough) approximation the flame height  $H$ .



# Turbulent premixed flames

## Turbulent flame speed $s_T$

Turbulent flame speed  $s_T$  is effective propagation velocity of premixed flame in turbulent flow field.

### Necessary for calculation:

- Relation for  $s_T$  as function of
  - flame parameters (fuel, stoichiometry,  $p$ ,  $T \rightarrow s_L$ )
  - Turbulence parameters ( $u'$ ,  $L_x$ ,  $Re_t$ ,  $Da$ , ...)

Is discussed in literature with several different approaches:

- **Theory (Damköhler 1940):** For wrinkled laminar flame surfaces the turbulent reaction rate and thus also the turbulent flame speed is proportional to geometrical flame surface area

$$\frac{s_T}{s_L} = \frac{A_L}{A_T} = 1 + \frac{u'}{s_L} \quad (6.16)$$

# Turbulent premixed flames

## Turbulent flame speed $s_T$

Measurements of flame propagation in turbulent stirred ignition bomb experiments (Bradley et al.): **Correlation from Gülder (1990)**

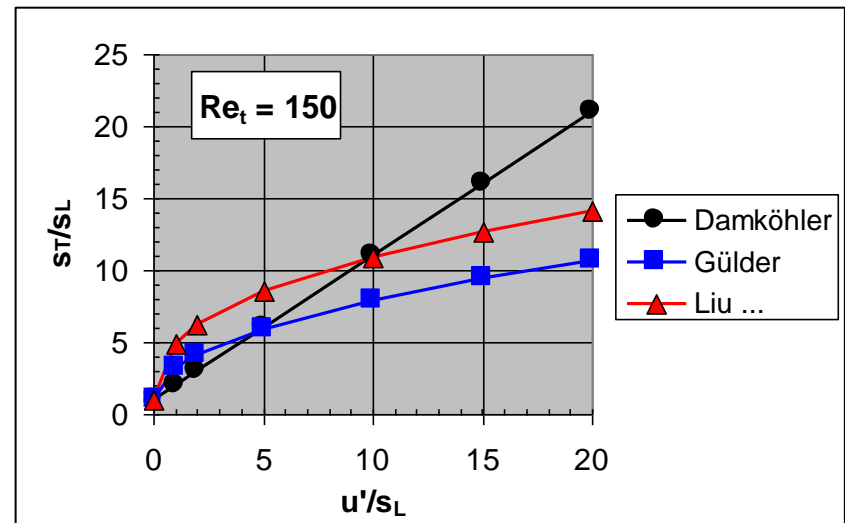
$$\frac{s_T}{s_L} = 1 + 0,62 \left( \frac{u'}{s_L} \right)^{0,5} \cdot (Re_t)^{0,25} \quad (6.17)$$

Measurement of normal component  $u_n$  directly before the flame front as function of turbulence and flame parameter **from Liu et al. (1993)**

$$\frac{s_T}{s_L} = 1 + 0,435 \left( \frac{u'}{s_L} \right)^{0,4} \cdot (Re_t)^{0,44} \quad (6.18)$$

**Zimont (1995)** (for  $u' > s_L$ ),  $A = 0,5 \dots 1$

$$\frac{s_T}{s_L} = A \cdot Pr^{1/4} \cdot Re_t^{1/4} \cdot \left( \frac{u'}{s_L} \right)^{1/2} \quad (6.19)$$



# Turbulent premixed flames

## Calculation of turbulent premixed flames

- Numerical calculation procedure for turbulent premixed flames is difficult
- **Aim: Combustion model to be coupled to computational fluid dynamics (CFD)**
- Not yet for practical applications, current research topic
- Possible approach:

Borghi diagram shows:

**Typical: Wrinkled thin flame fronts, locally similar to laminar, if  $Ka < 1$**

(Measurement (--> LTT) shows, even if  $Ka < 10 \dots 100$ )

**then ...**

# Turbulent premixed flames

## “Flamelet“ –Approach: *Peters 1986*

For **laminar-like** wrinkled flame fronts a **decoupling** is possible between turbulence and reaction :

- Turbulent flow field wrinkles the flame
- Reaction remains similar as in laminar case (maybe modified from curvature or strain effects)

**Flamelet-approach simplifies numerical calculation significantly !**

Calculate basically the place of reaction (averaged), while the detailed chemistry is known from laminar flames.

# Turbulent premixed flames

## “Flamelet” – Approach

for that introduce a mean reaction progress variable  $\bar{c}$

$$\bar{c} = \text{Probability to find burnt gas} \left( \text{remember : } c = \frac{T - T_0}{T_{\max} - T_0} \right)$$

For this variable basically one balance equation is enough instead of  $N$  equations for energy and species.

This equation can be calculated numerically together with the flow field (+ turbulence model).

Several approaches for this  $c$ -equation (**sometimes also called  $G$ - or  $\Sigma$ -equation**) are discussed in the literature

One approach, based on turbulent flame speed, gives e.g. (*Dinkelacker, Helbig, Hölzler 1999*): (next page)

# Turbulent premixed flames

## Example for Flamelet-Model **Turbulent-Flame-Speed-Closure (TFC)**

### Idea:

- Average reaction rate  $\sim$  Turbulent flame speed
- This yields a "Turbulent-Flame-Speed-Closure" for averaged reaction term (Zimont & Lipatnikov 1995)

$$\bar{w}_c = \rho_u \hat{s}_T(x) \cdot |\nabla \bar{c}| \quad (6.21)$$

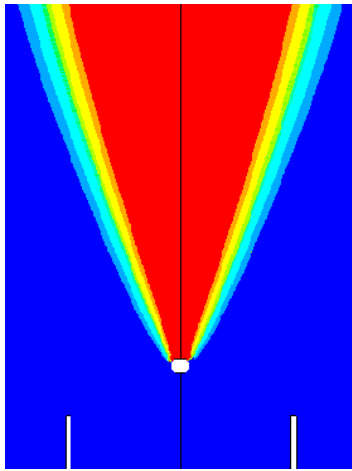
place of reaction

- **Turbulent burning velocity**, e.g., from equation (6.19), for application with pre-factor of  $A = 0,52$  (Zimont & Lipatnikov 1995)
- Solution as subroutine with standard-CFD-program (e.g., Fluent)

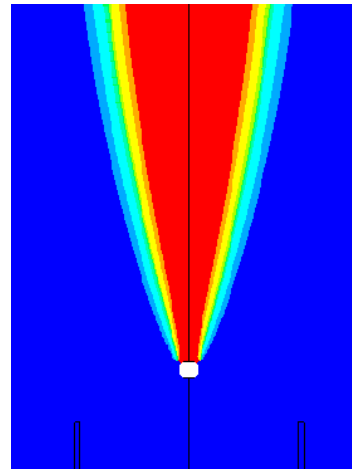
# Turbulent premixed flames

Testcase: turbulent premixed V-flame: Reaction progress  $\bar{c}$

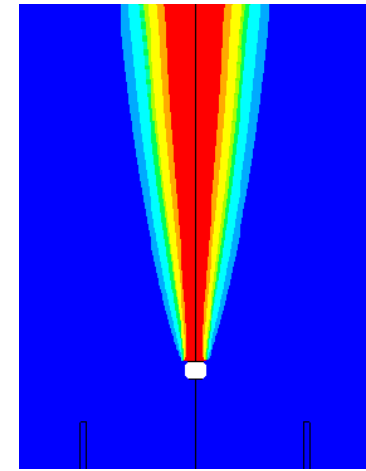
*Simulation*



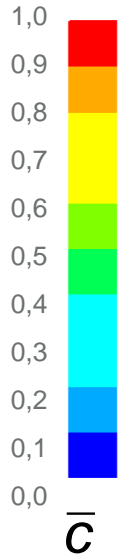
$\lambda = 1.43$



$\lambda = 1.72$

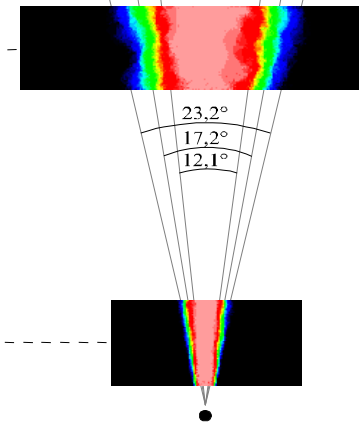
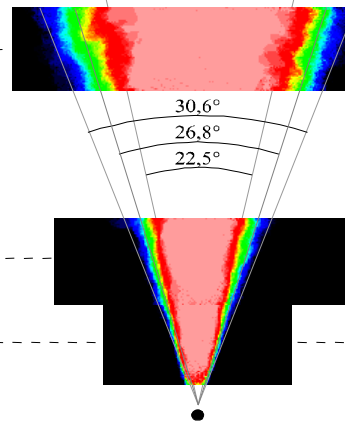
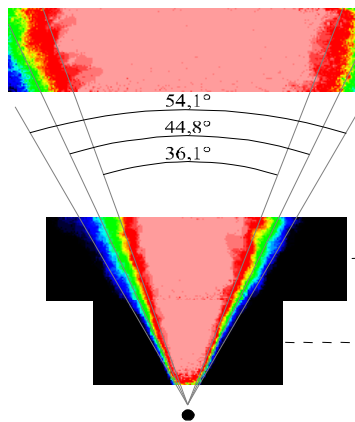


$\lambda = 2.00$



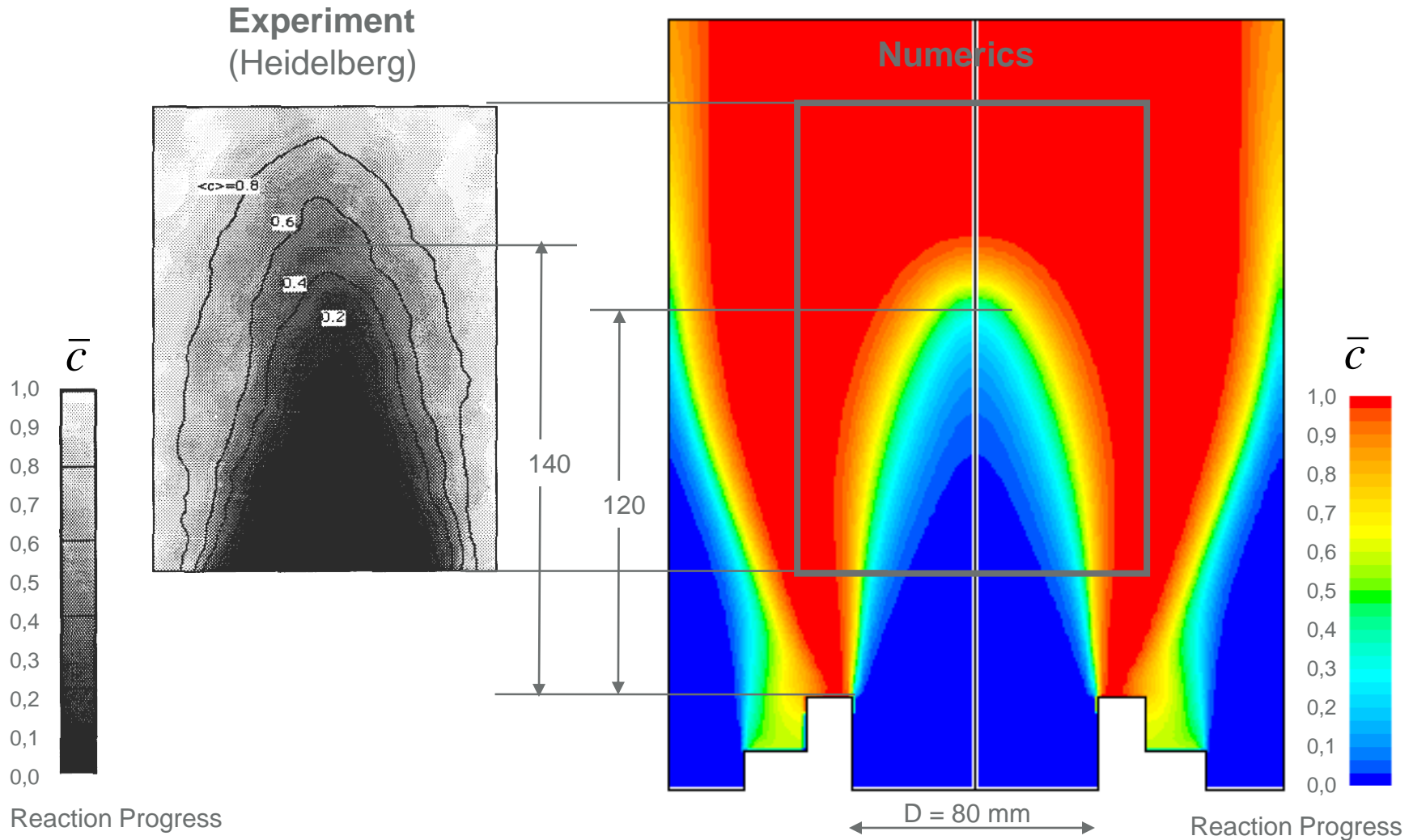
*Experiment*

2-dim. Rayleigh-  
Thermometry (A.  
Soika)



# Turbulent premixed flames

## Testcase: 80 mm - Bunsen Flame



# Turbulent non-premixed flames

## 6.3 Turbulent non-premixed flames

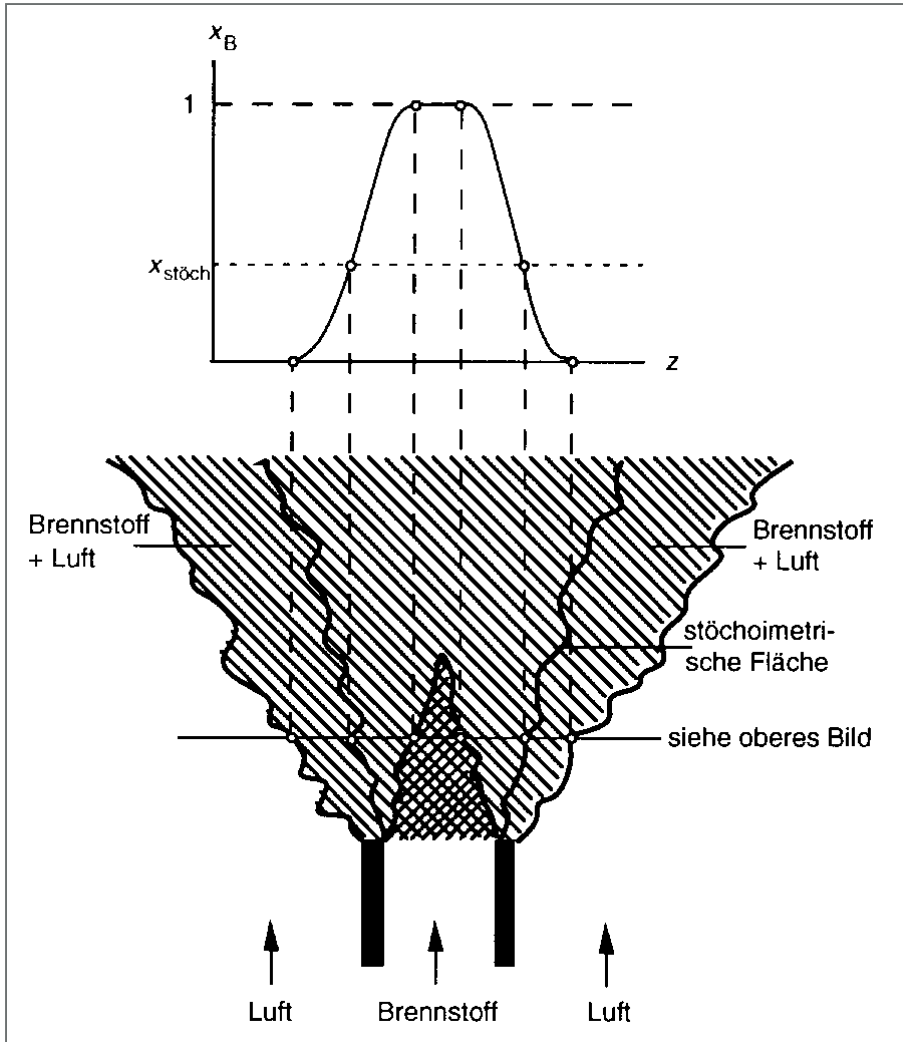
- Fuel and air are mixed in burning chamber
- Turbulence supports mixing
- Large practical relevance
- Also for solid and liquid fuels
- Disadvantage: More pollutants and soot as premixed flames

**3.1 Examples**

**3.2 Flame length**

**3.3 Mixture fraction-concept**

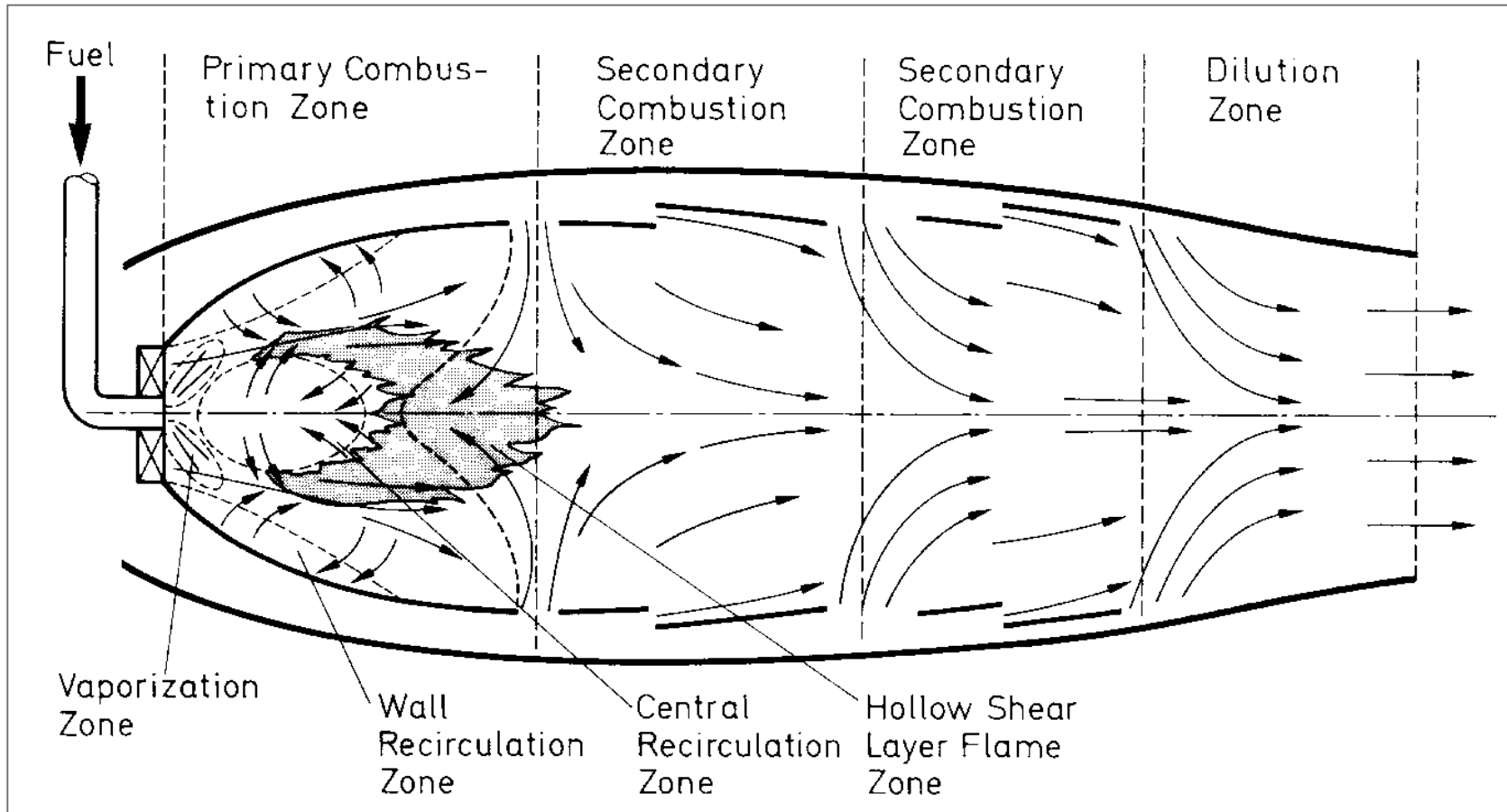
# Turbulent non-premixed flames



Snap-shot of a turbulent jet-diffusion flame (schematics)

# Turbulent non-premixed flames

## Example: Burning chamber of air gas turbine (schematic)



Use of non-premixed (diffusion) flames owing to safety reasons (flashback)

# Turbulent non-premixed flames

## Mixture fraction concept

### Numerical calculation of diffusion flame

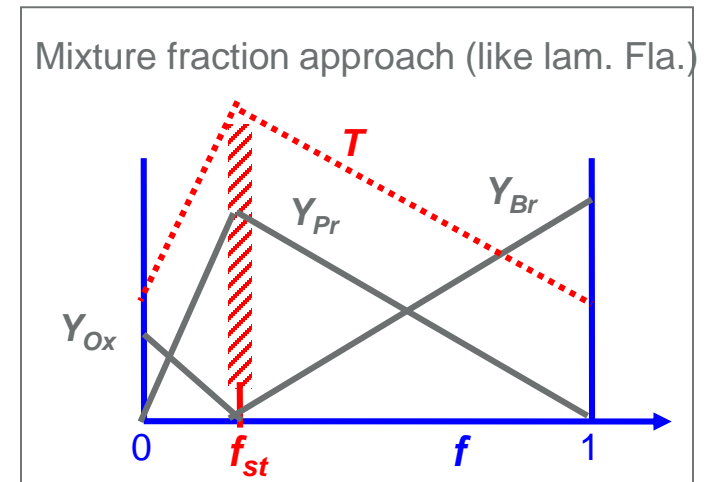
**Aim:** Numerical calculation of flame location and flame length.

**Models for diffusion flames often are based on observation, that mixing controls the reaction.** Then the **flow field couples with mixture fraction  $f$** ; to be calculated instead of species and temperature:

- Flow field, averaged ( $\bar{u}_i, \bar{p}$ )
- Turbulence field ( $k, \varepsilon$ )
- Mixture fraction field ( $\bar{f}, f'$ )

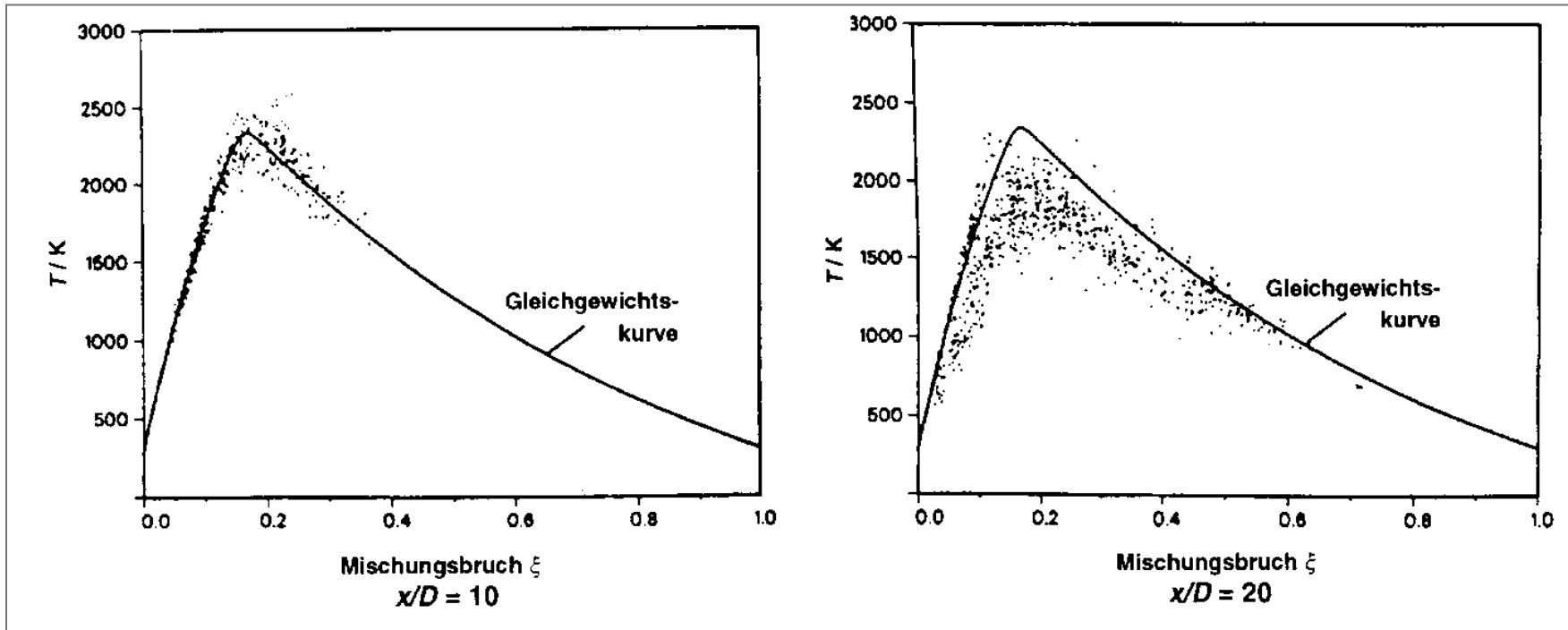
Allocation only once (ideal situation, see -> )

- $\bar{f}, f'$  → Temperature field  
→ Heat release  
→ Species distribution



# Turbulent non-premixed flames

## Mixture fraction concept



## Temperature as function of mixture fraction

Turbulent non-premixed hydrogen jet flame, left: low turbulence, right: higher turbulence intensity

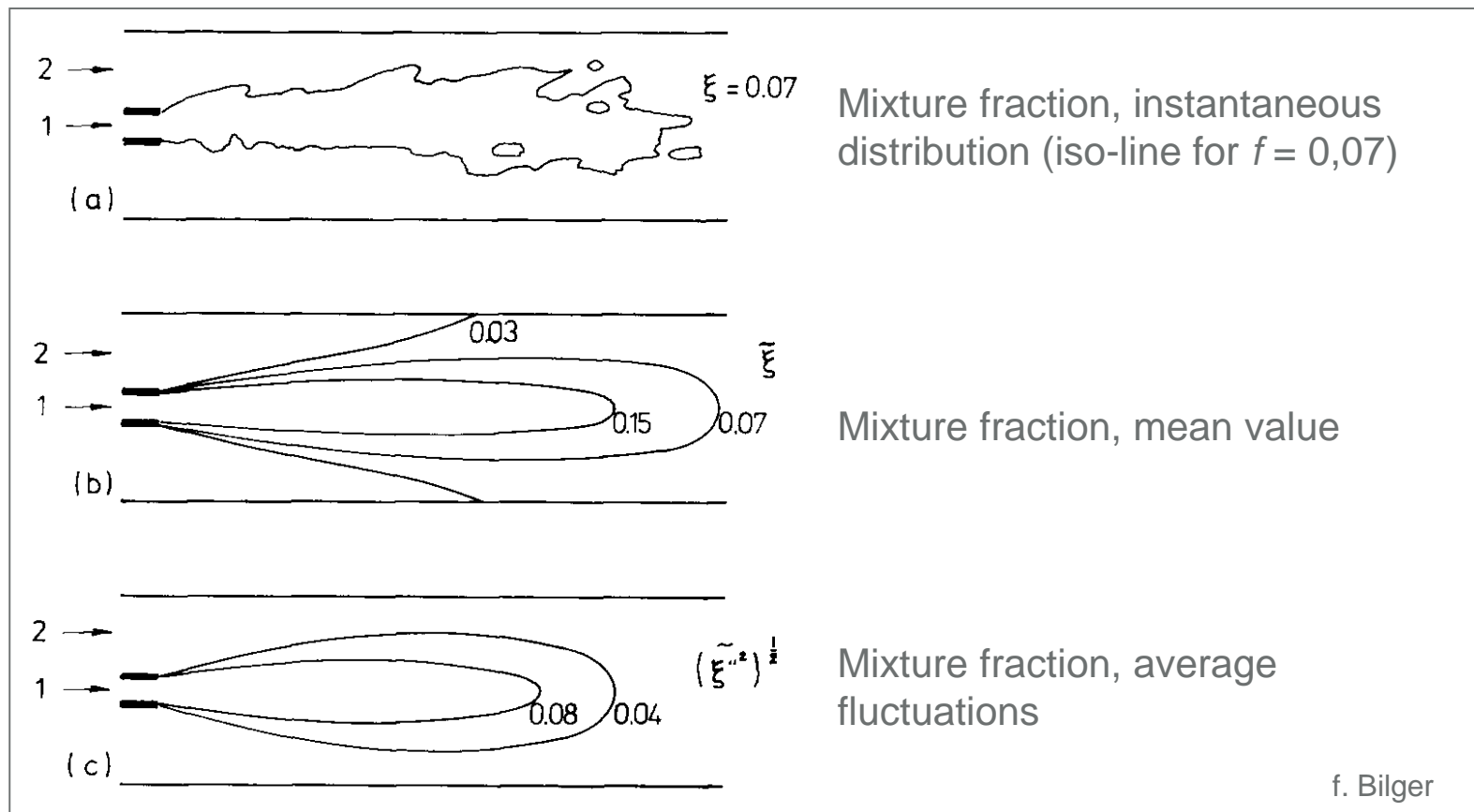
Measured (Laser-Raman-Scattering) vs. equilibrium calculation

(Magre, Dibble 1988, cit. after Warnatz et. al. 96)

# Turbulent non-premixed flames

## Mixture fraction concept

Example: Mixing field of a typical non-premixed turbulent flame



## Turbulent combustion to enhance mixing

- Turbulence-Flame Interaction
- Two extreme cases allow 'separation' of turbulence and reaction:
  - 'Fast mixing limit' (Stirred reactor model):  
spatially homogeneous chem. reactions
  - 'Fast chemistry limit': Wrinkled laminar 'flamelet'  
'flamelet' - approach

## Turbulent premixed flames

- Typically: fluctuating wrinkled thin flame **fronts** result in a broad flame **brush**
- Turbulent flame speed  $s_T$
- **Flamelet models** for calculation

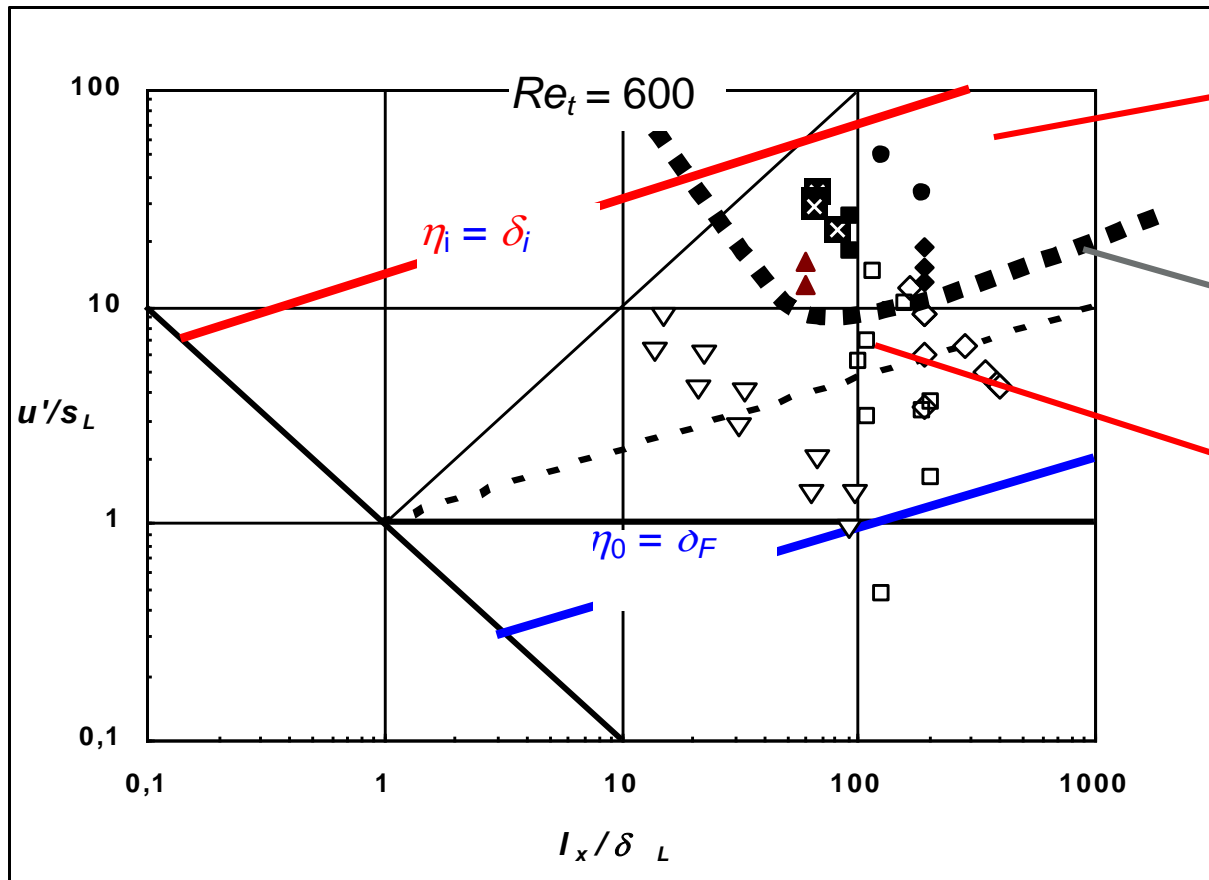
## Turbulent diffusion flames

- Turbulence enhances fuel-air mixing
- Mixture fraction concept

# Turbulent premixed flames

## Results of experiment of premixed turbulent flame structure

Range of wrinkled laminar-like flames (Flamelet) is more extended



Thin reactions zone,  
Locally modified  
preheat zone

No significant  
thickening  
(partly even thinned  
flames instead \*)

Details, see \*

\* Dinkelacker, 20. Deutscher Flammentag, VDI-Berichte Nr. 1629, S. 473 (2001)

# Turbulent premixed flames

## Turbulent flame speed $s_T$

fol. Bradley,

24. Comb. Symp. (92):

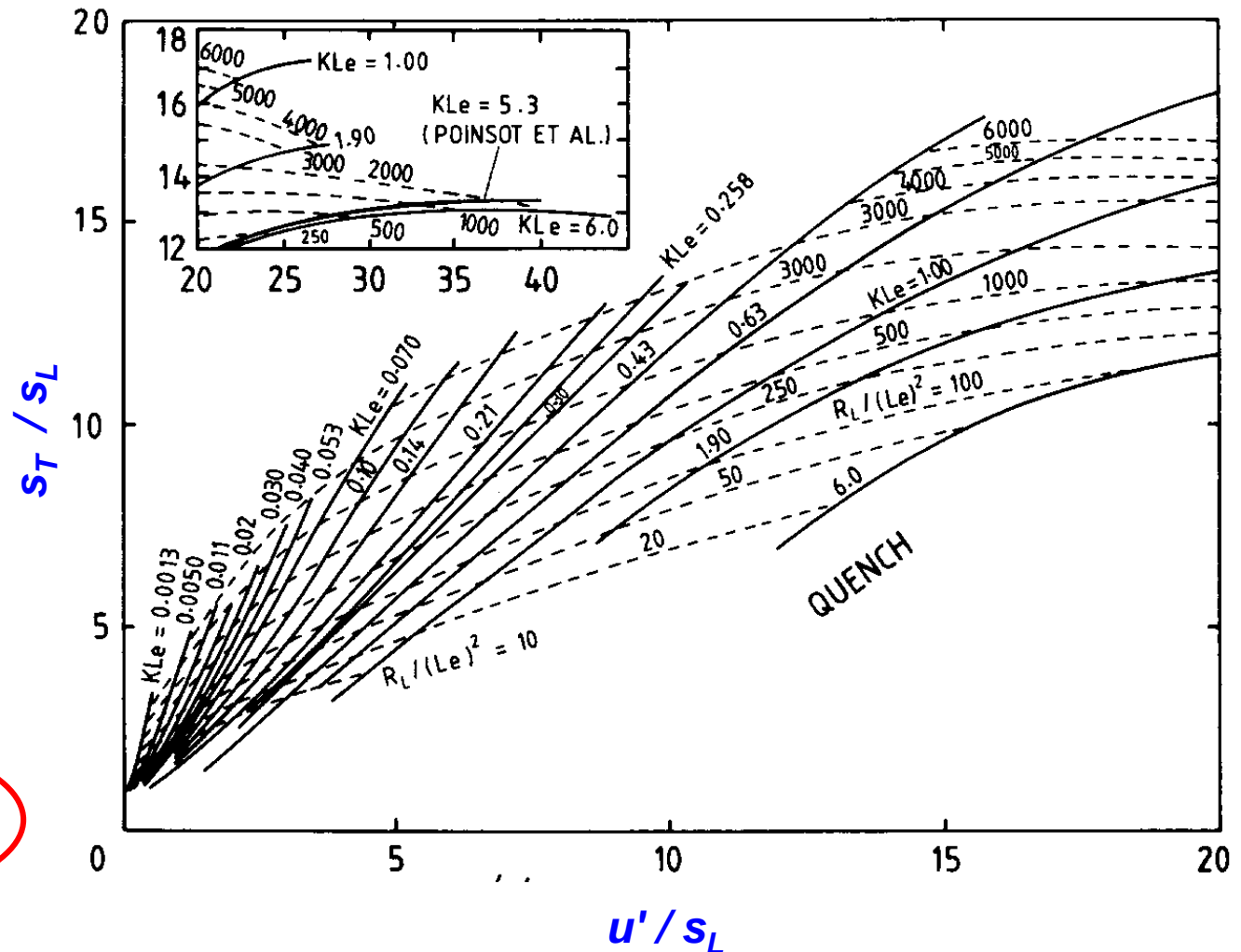
$R_L$  = turb. Reynolds number

$Le$  = Lewis number

$K$  = dimensionless

Strain rate

$$K = \left( \frac{a}{s_L / \delta_L} \right) = \left( \frac{u' / \lambda}{s_L / \delta_L} \right)$$



$s_T / s_L$

$u' / s_L$

Critics:  
Measured flames  
have been very small

# Turbulent premixed flames

## Turbulent flame speed $s_T$

For increasing turbulence ( $u'/s_L$ ) the turbulent flame speed increases slower ("*Bending Effect*").

### Possible reasons:

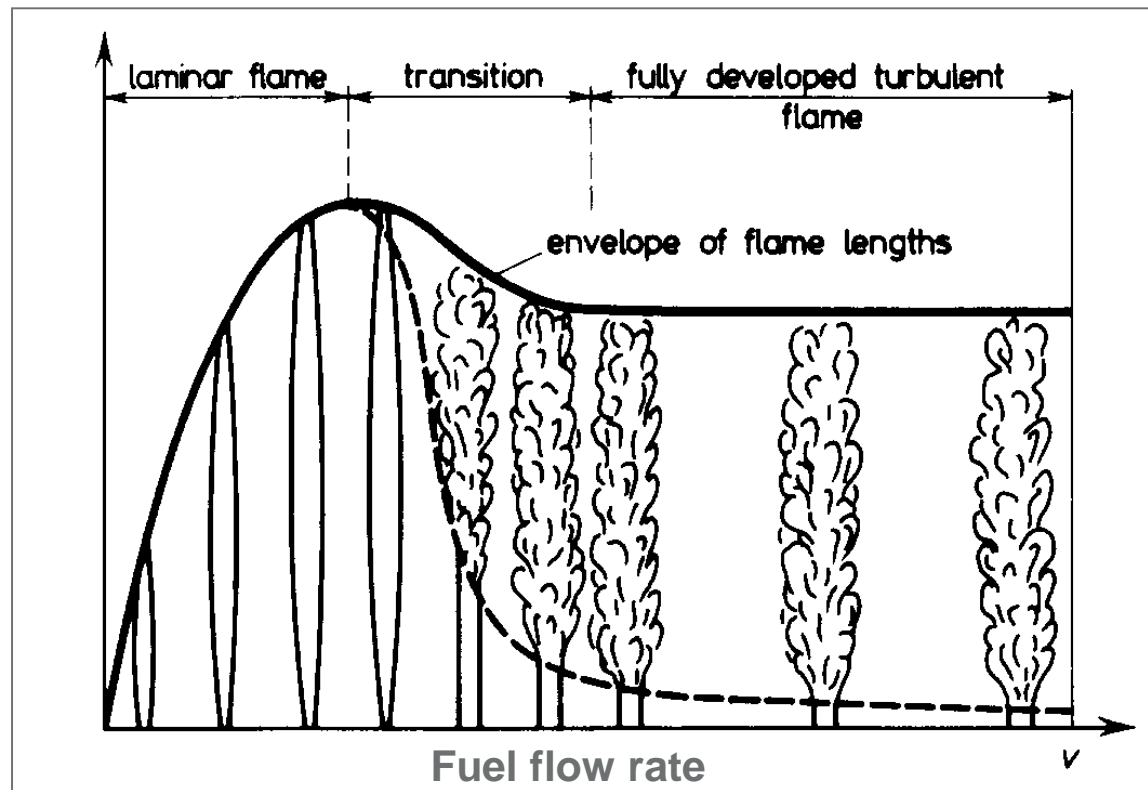
- Flame area increases not with  $u'/s_L$ , but annihilates due to interaction
- Reaction locally reduced compared with "laminar flamelets", due to
  - local curvature
  - Influence of small scale eddies
  - local breaks in reaction front (flame quench) ?

For further increase of  $u'/s_L$  flame quenches totally.

# Turbulent non-premixed flames

## Length of turbulent jet non-premixed flames

Length of flame nearly independent on fuel exit velocity, for developed turbulent flame



# Turbulent non-premixed flames

## Length of turbulent jet non-premixed flames

### Empirical relation for flame length of turbulent jet non-premixed flame

(Delichatsios 93, Turns 96)

Length of diffusion flame is controlled by mixing. From that the following relation is derived for jet flames (here for "sufficiently" large momentum of the fuel flow, buoyancy is neglected, calm surroundings; for other conditions see Turns 96).

$$L_f = \frac{23 \cdot d_j \cdot \left( \frac{\rho_B}{\rho_L} \right)^{1/2}}{Y_{B,st}}$$

(6.20)

Flame length  $L_f$

Diameter of fuel inlet  $d_j$

Density ratio between fuel and air  $\rho_B/\rho_L$

Stoichiometric fuel mass fraction  $Y_{B,st}$  (Lecture 2, Table 2.1)

### Note:

Length of flame is (approx.) independent of inlet velocity !

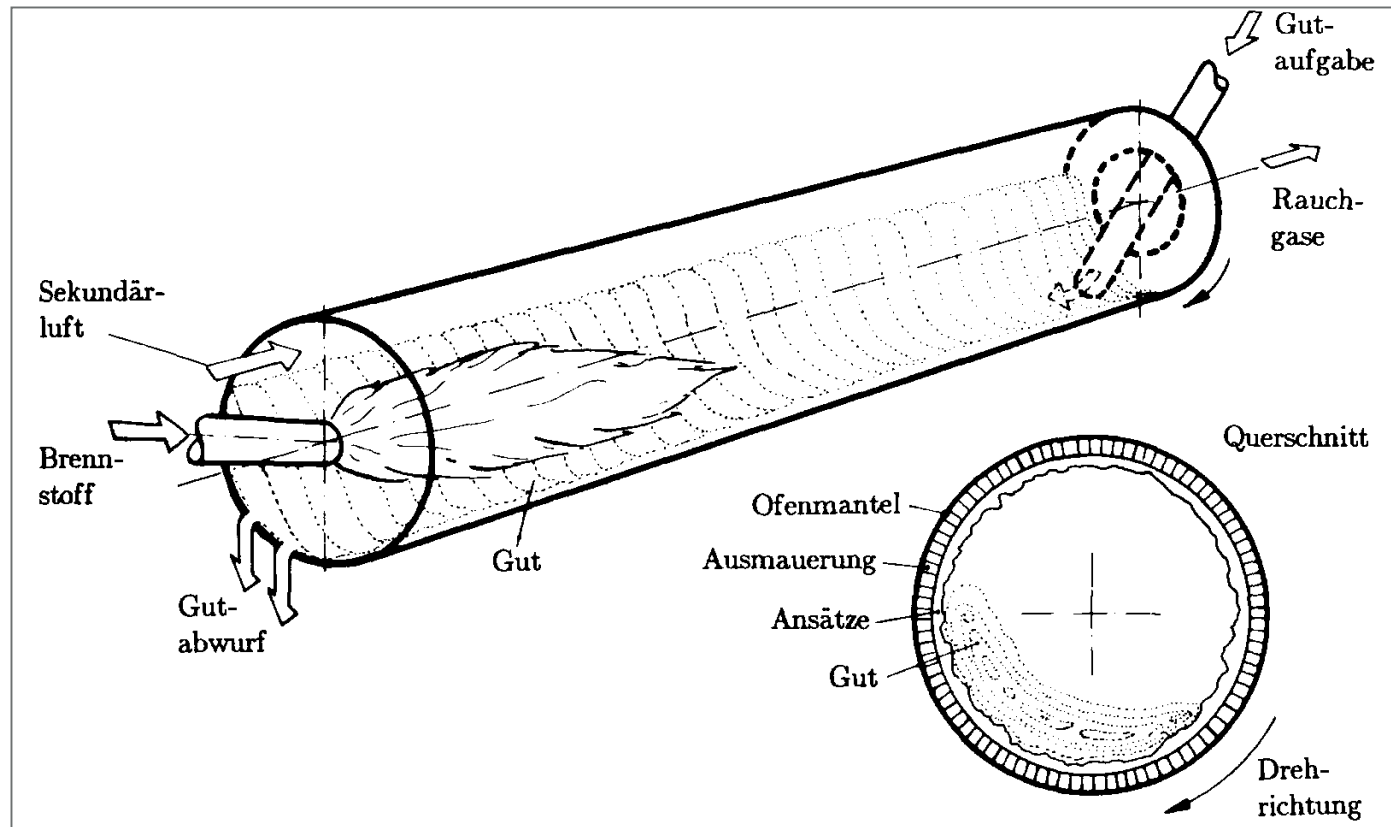
Length of flame is proportional to diameter of inlet!

Length of flame depends on fuel

**Example:** Methane in air,  $d_j = 10$  mm, gives length  $L_f = 3,1$  m

# Turbulent non-premixed flames

## Example: rotary furnace



Turbulent diffusion flame in rotary furnace for production of cement

(n. Görner)



(**Assumption:** fully developed turbulence, homogeneous, isotropic)

Turbulent fluctuation velocity

$$u' = u_{rms} \quad \text{(measured)}$$

Integral length scale (Macro length)

$$L_x \quad \text{(measured)}$$

Turbulent Reynolds number

$$Re_t = u' L_x / \nu \quad (6.7)$$

Kolmogorov length (Micro length)

$$\eta = L_x / Re_t^{3/4} \quad (6.8)$$

Increase of turbulent Reynolds number broadens turbulence spectrum

